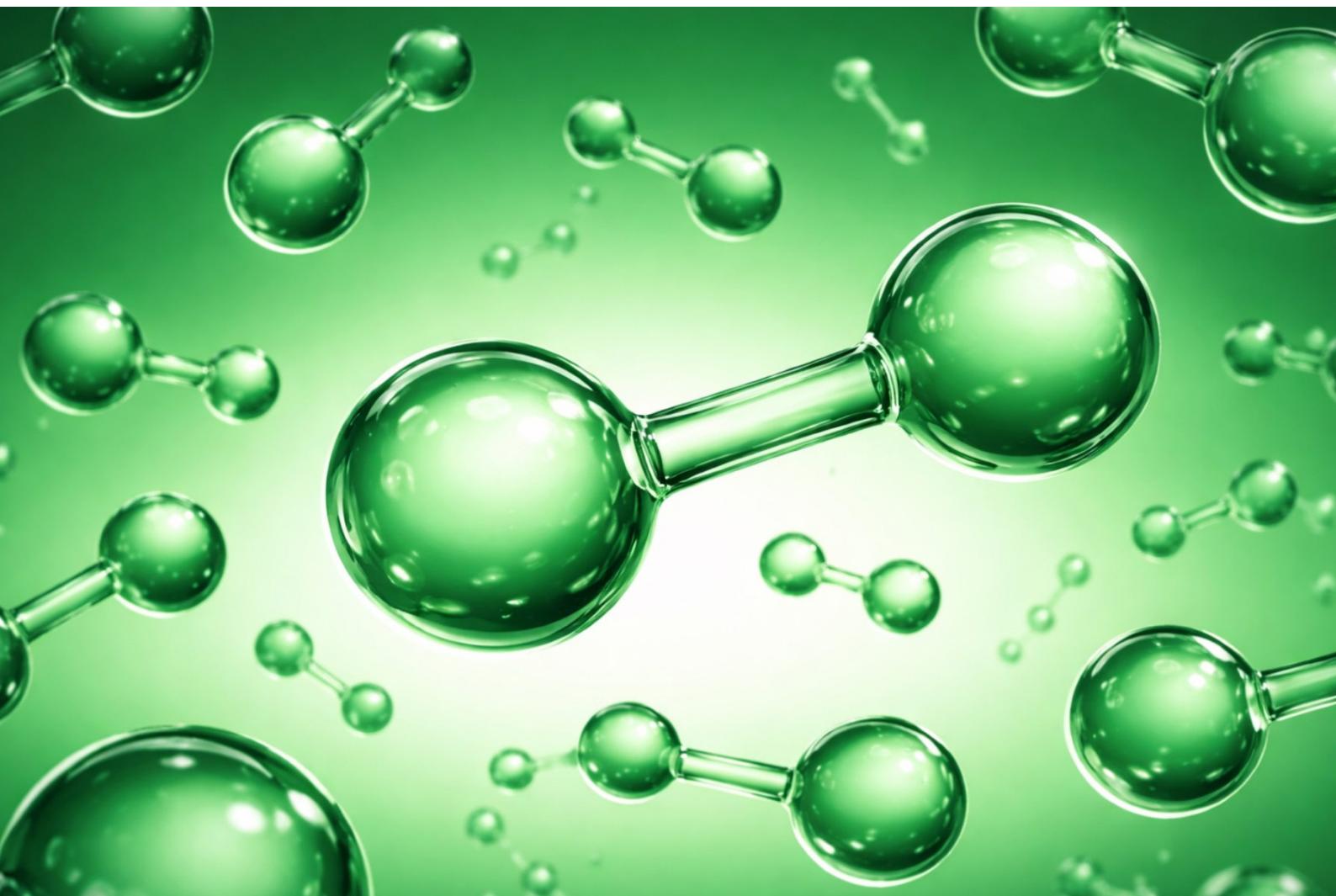


DEAD AND BURIED

Why our green hydrogen
hope is gone for good

Jude Blik, Aidan Morrison





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hope is gone for good**

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THE CENTRE FOR
INDEPENDENT
STUDIES

Analysis Paper 101

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Executive Summary

Green hydrogen is often heralded as a cornerstone of Australia's net zero ambitions, but the reality is that it is not viable today, and won't be in the foreseeable future. This paper examines the reasons green hydrogen will likely remain prohibitively expensive, why projects are stalling, and how the recently announced Orica subsidy exposes Australia's strategy as untenable.

Hydrogen is intended to play a critical role in Australia's decarbonisation plans. Beyond replacing grey hydrogen (produced from natural gas) in chemical manufacturing, green hydrogen — produced via electrolysis using renewable energy — is envisioned for advanced applications like green metals production, long-haul transport, and electricity grid support.

However, green hydrogen's high production costs and operational challenges threaten these ambitions. The fundamental issue lies in the energy-intensive nature of electrolysis. Producing 1kg of green hydrogen requires 53 kWh of energy — equivalent to powering a typical home for 3 days. This energy demand, coupled with high capital costs for electrolyzers, makes green hydrogen expensive.

Grid-connected electrolyzers can theoretically operate at high utilisation rates, but face costly firmed electricity prices, while renewable-connected systems designed to absorb surplus solar power would suffer from low utilisation rates aligned with renewable capacity factors.

Sensitivity analyses show that even with optimistic assumptions around future costs of technology or electricity, green hydrogen costs realistically exceed \$10/kg, far above the \$2/kg market price of grey hydrogen. This gap necessitates subsidies of approximately \$8/kg to compete, a scale that becomes astronomical when applied to national or export ambitions.

The challenges extend beyond production. Applications like long-haul transport and steelmaking require storage and transportation, which are hindered by hydrogen's high compression or liquefaction

costs (12–36% of energy content). Fuel cell applications for transport must grapple with a round-trip energy efficiency below 30%, and hydrogen's volatility and embrittlement of metals increase safety and maintenance costs. These factors further erode the economic case for hydrogen in hard-to-electrify sectors.

The Orica deal exemplifies the exorbitant cost of green hydrogen. The NSW and federal governments' \$547 million subsidy for just 4,700 tonnes of hydrogen annually — 7.5% of Orica's current usage — equates to \$10.99/kg in subsidies, far exceeding the government's \$2/kg Hydrogen Production Tax Incentive. This implies a carbon abatement cost of \$915–\$1,569/tonne CO₂, 26–44 times higher than the price of Australian Carbon Credit Units (ACCUs) at \$30–\$40/tonne. Scaling this to replace Orica's full hydrogen needs would require \$7.3 billion — close to the market capitalisation of the entire company. At this rate, replacing Australia's 500,000 tonnes of annual industrial hydrogen use would require \$58b in subsidies, while producing 15 million tonnes for green energy exports could demand \$3.19 trillion.

The reliance on subsidies, even for the simplest use case of on-site chemical production, suggests that more complex applications are even less viable. The Orica project exposes a push to prop up a technology whose costs are driven by immutable physical constraints, raising serious questions about the feasibility of Australia's green hydrogen strategy.

It is essential that Australia removes unrealistic assumptions about green hydrogen from official plans, including the Integrated System Plan, to prevent us committing today to investments and strategies which have no real prospect of success.

Introduction

Hydrogen has been 'the future' at least four times. The simplest of elements, it appears to have an intoxicating allure to the modern mind, capable of generating sequential waves of official enthusiasm about its potential, without any of the expectations coming to fruition. A single proton-electron pair, coupled up to form molecules of H₂ has an array of eye-opening properties. It is extremely light — the lightest thing in existence — and can burn with, or otherwise combine with, oxygen to release vast amounts of energy. By mass, it has the highest energy density of any chemical — 120MJ/Kg — more than double that of diesel.

But the juxtaposed energy density with physical un-density has made the hydrogen hard a difficult one to play into many practical applications. A few other eccentric chemical properties, such as the capacity to embrittle metals, and burn at extreme speeds and temperatures, add to the challenges.

The first hope for hydrogen was for it to be the lift-gas that would enable the airship, by which "man will crown his conquest of the air".¹ In 1930, the British Labour Air Minister Lord Christopher Thomson dreamed up the Imperial Airship Scheme to connect the far-flung outposts of the British Empire through the new medium of the air.² Yet Thomson was tragically killed on R101's first overseas voyage to India in October 1930, when the ship crashed in France, killing 48 of the 54 people on board.³ A few years later in 1937, the Hindenburg burned over Lakehurst, New Jersey.⁴ The technology had enjoyed enormous official backing and utopian rhetoric, but mass uptake never arrived, particularly as airplanes had grown in popularity and taken over long-distance travel.

Hydrogen saw another 'false dawn' in the 1970s,⁵ a decade in which oil shocks and concerns about fossil fuel depletion in the face of exponential growth in global primary energy use were at the fore.⁶ In 1970, the electrochemist John Bockris coined the term 'hydrogen economy' during a discussion at the General Motors Technical Center in Warren, Michigan, envisioning a future in which hydrogen was

used as an alternative to fossil fuels.⁷ The year after the 1973 oil crisis, The Hydrogen Economy Miami Energy Conference saw 750 participants from 80 countries gathered to promote hydrogen as an energy source, which led to the creation of the International Association for Hydrogen Energy.⁸ The International Energy Agency was established in 1974, with a key aim to respond to the global oil crisis by exploring alternative technologies such as hydrogen, with nuclear energy widely considered as an option to produce both electricity and abundant and cheap hydrogen.⁹ But interest in hydrogen once again waned, as the oil embargo lifted, new fossil fuel sources were exploited and oil prices fell.¹⁰

The hydrogen dream came back with a vengeance once again in the 'false dawn' of the 1990s and 2000s. In the late 1990s, automobile and power companies were spending billions in pursuit of making cars that could "go 5000 miles between fill-ups" and electric power plants you could "buy like appliances".¹¹ In his 2003 State of the Union address, George W. Bush launched a US\$1.2b Hydrogen Fuel Initiative, promising that "with a new national commitment, our scientists and engineers will overcome obstacles... so that the first car driven by a child born today could be powered by hydrogen, and pollution-free."¹² But by 2009, the Obama administration was slashing hydrogen car funding. Energy secretary Steven Chu explained the U-turn in strikingly plain language: "We asked ourselves, 'Is it likely in the next 10 or 15, 20 years that we will convert to a hydrogen car economy?' The answer, we felt, was 'no'."¹³ This prediction turned out to be correct — since then, less than 20,000 hydrogen cars have been sold across the US, mostly being confined to California where taxpayer funding supported the development of public fuelling stations.¹⁴

Despite the failure of a 'hydrogen economy' to emerge after decades of grand promises and boatloads of funding, Australian policymakers have not proven immune to hydrogen's spell. One key recent example of this is the subsidy package given to Orica's Kooragang Island facility in the Hunter Valley. In contrast to transformational visions of transport and electricity, this

facility epitomises some of the mature industrial use-cases of hydrogen, namely the production of ammonia for use in fertiliser and bulk explosives. On July 4, 2025, Chris Bowen announced a \$432m federal subsidy for green hydrogen to replace just 7.5% of the natural gas used to produce hydrogen at the plant.¹⁵ Orica had previously received \$45m from the New South Wales government,¹⁶ and \$70m from the federal government¹⁷, bringing the total for the project to \$547m.

In the history of hydrogen subsidies, half a billion dollars may not even raise eyebrows, let alone concern. But those unfamiliar with the more technical aspects of the net zero plan — and particularly green hydrogen's role in the energy transition — will miss

the alarming reality exposed by the scale of this subsidy, for such a small impact on an existing use-case for hydrogen. By the numbers, this announcement is the most damning indictment of Australia's energy transition plan to-date.

To understand why, we must first understand green hydrogen's role in Australia's net zero plan — the hopes and dreams held for hydrogen in a decarbonised future. We must also identify the fundamental physical challenges in the production of hydrogen that make it permanently expensive, as 'false dawn' after 'false dawn' has proven. Understanding hydrogen's designated role in the energy transition and its fundamental physical attributes will reveal why the Orica deal exposes those challenges.

1. Hydrogen is the panacea we are relying on to make net zero work

For over 100 years, hydrogen has been a vital feedstock for industrial chemical production. It is generally made from methane in a process known as steam reforming, and combined with nitrogen to produce ammonia, which is then used to produce fertilisers, explosives, and numerous other chemicals. In Australia, about 500,000 tonnes of hydrogen is currently produced annually for these uses.¹⁸ This accounts for roughly 1% of the nation's total greenhouse gas emissions.¹⁹

But future uses for hydrogen are far more expansive than these relatively minor applications. In a decarbonised world, 'green hydrogen' produced by electrolysing water with renewable energy is intended to replace 'grey hydrogen' made from natural gas, not only in ammonia production for fertilisers and explosives, but for a variety of other applications. These uses are increasingly baked into official planning documents.

The so-called 'energy transition' has three main challenges:

- Decarbonising the electricity grid;
- Electrifying other sources of emissions;

- Abating or otherwise offsetting the hard-to-electrify sources of emissions.

Hydrogen is touted as the future fuel for the third of these challenges. The National Hydrogen Strategy outlines the role that hydrogen plays in the government's net zero plans.²⁰ Its many uses include green metals production, long haul transport, and power generation for the grid.

CSIRO and Climateworks estimate that in 2050, hydrogen will make up 3–4% of final energy demand across NEM-connected states (16% in a hydrogen export scenario),²¹ with many advocates such as the Superpower Institute advocating for extensive use in industry to create energy-intensive processed products for export as part of a 'green superpower' strategy.²²

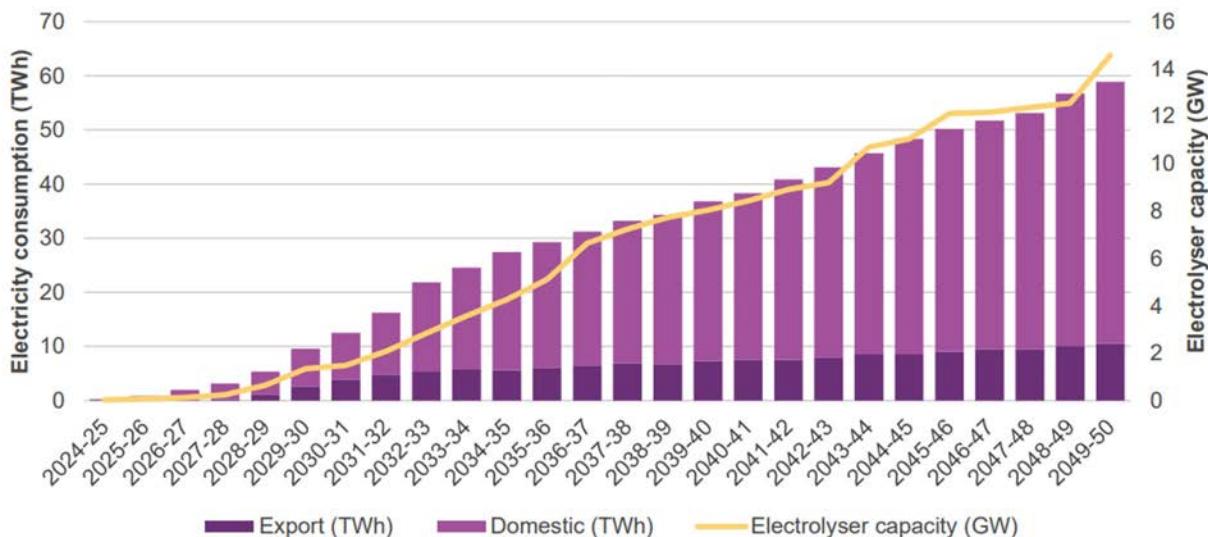
The past half-decade of AEMO's Integrated System Plan (ISP) — Australia's official energy transition plan for the electricity grid — documents show a journey toward greater use of hydrogen.

The ISP first mentioned hydrogen in 2020 as having "the potential to meet some of Australia's energy needs, once it is economically competitive and the possible

challenges to efficient sector integration are resolved", but the plan did not attempt a quantitative analysis of its use in the energy system "as the industry remains in the early stages of development".²³

The 2022 ISP was the first to include a specific 'Hydrogen Superpower' scenario, where extra electricity demand is modelled for hydrogen production, to export supposedly abundant renewable energy.

Figure 1 - AEMO ISP - Electricity consumption associated with hydrogen production and ammonia conversion, Step Change

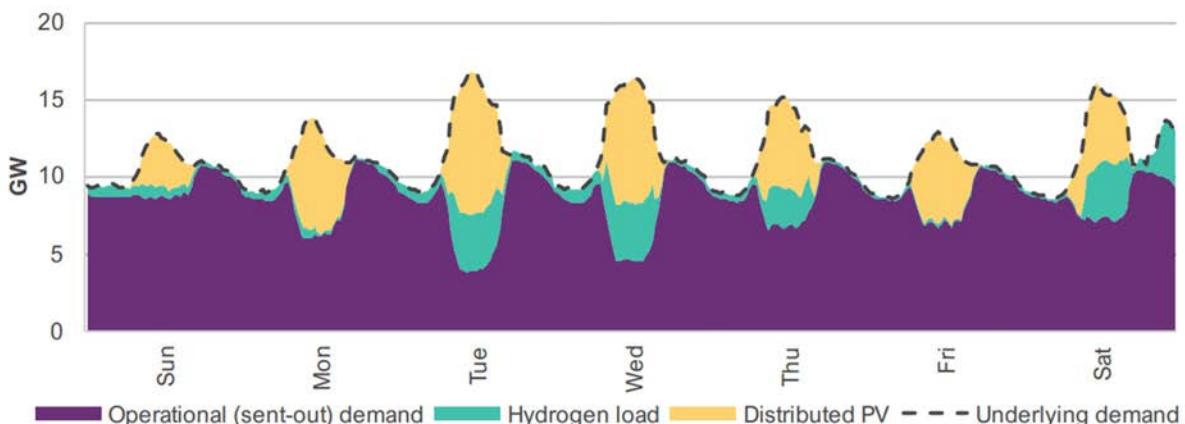


In particular, a 'solar soak' role begins to be modelled in the grid, with "large industrial users, including hydrogen production ... set to take most advantage of surplus renewable generation when it is available, particularly during daylight hours".²⁶ The

Even outside this scenario, hydrogen is considered as a potential fuel for both grid and transport.²⁴

In the 2024 ISP, hydrogen's role was significantly expanded to include its use in all scenarios to varying extents. Even the 'Step Change' scenario, presented as the central case, assumes significant electricity consumption for hydrogen production (Figure 1).²⁵

Figure 2 - AEMO ISP - Projected week of hydrogen electrolyser load in Queensland in 2040, Step Change (GW)



As seen in Figure 2, the utilisation rate of hydrogen electrolyzers regularly falls close to zero. Hydrogen electrolyzers are

ISP assumed electrolyzers would "operate flexibly, potentially reducing electricity consumption when renewable energy resources are limited ... and consuming more during daylight hours when excess solar energy is abundant".²⁷

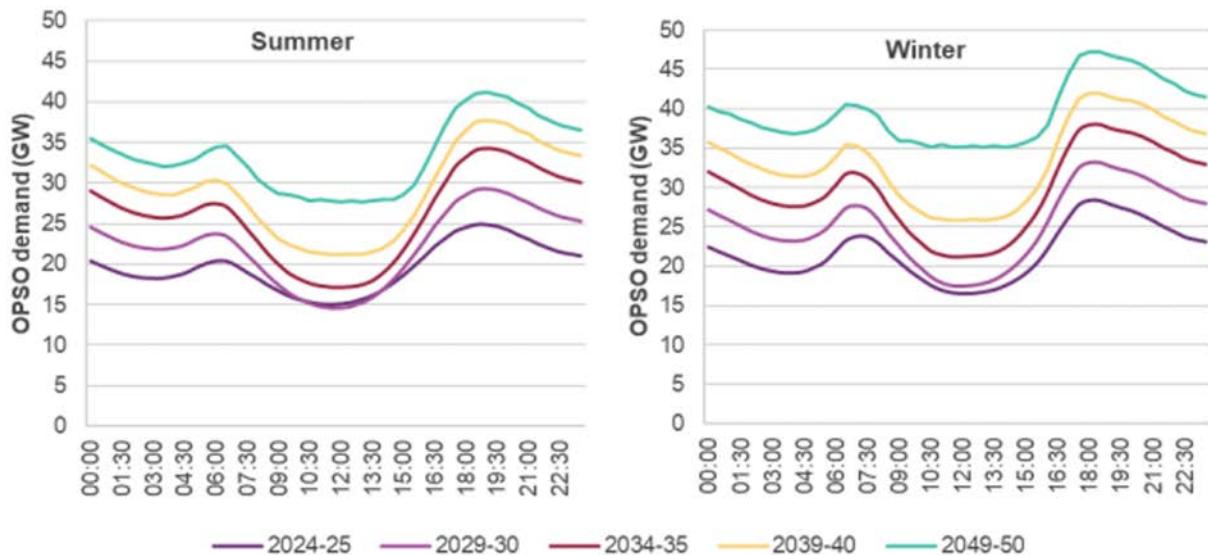
modelled as being available to soak up excess solar output and can switch off during periods of low generation:

Hydrogen load in this ISP modelling is therefore expected to lift minimum demand and have minimal impact at times of peak demand. It is also expected to be technically capable of providing flexibility by turning off for whole days when weather conditions are unfavourable, depending on the commercial implications of doing so.²⁸

In the AEMO plans, the role hydrogen plays is not simply an extra way to use cheap power, but a critical part of system stability. Appendix 4 of the 2024 ISP noted that "during summer, demand profiles exhibit lower midday troughs due to higher distributed PV output".²⁹ This presented an issue of a large gap between the demand

and supply of power in the middle of the day, since this is also when grid-scale solar is at its peak output. If demand does not match supply, the system breaks down. The ISP solved this problem by forecasting large increases in demand from hydrogen production, noting that "in the absence of hydrogen production, the average midday summer demand would be only 15 GW in 2049-50".³⁰ These hydrogen loads are not trivial, but represent roughly 15 GW of peak demand.³¹ Figure 3 demonstrates that the planned average summer demand is between 25 and 30 GW.³² This means that without hydrogen, the system could be facing instances where only 50% of generation is met by demand — a critical stability risk.

Figure 3 - AEMO ISP - Operational sent-out demand average time-of-day forecasts, summer and winter, Step Change



Not only are these electrolyzers forecast to operate infrequently (when the sun shines), but also seasonally — contributing more to the demand gap in summer than in winter. This must necessarily result in minuscule utilisation rates. However, hydrogen electrolyzers are capital-intensive, and maintaining high utilisation rates is key to their profitability. Likewise, most industrial manufacturing requires steady-state operation. The ISP addressed these challenges in Appendix 2, and concluded, sensibly, that "higher electrolyser utilisation factors (90%) combined with daily hydrogen production requirements is forecast to need greater renewable energy and an even greater amount of utility-scale storage"³³ — all of which substantially raises costs.

It is clear hydrogen does not represent a minor part of our future energy system. It is not merely a bonus industry that could be enabled in a hypothetical future world of abundant green energy. Green hydrogen is intended to form a core part of Australia's future energy system, and play a critical stabilising role. Without it, the future grid that is being planned will not function. Yet the extent to which our official plans rely on hydrogen belies the major challenges facing the industry. The major recommendation of this paper is to heed the difficulty with which green hydrogen is currently being implemented, and remove the reliance on hydrogen from the government's energy system and net zero planning.

2. Yet things are not going well for hydrogen

Despite the global hype, green hydrogen projects are not keeping pace with hopes or expectations. Recent analysis by Rystad Energy indicates 99 percent of the announced capacity of hydrogen projects

have not progressed beyond the concept or approval stage.³⁴

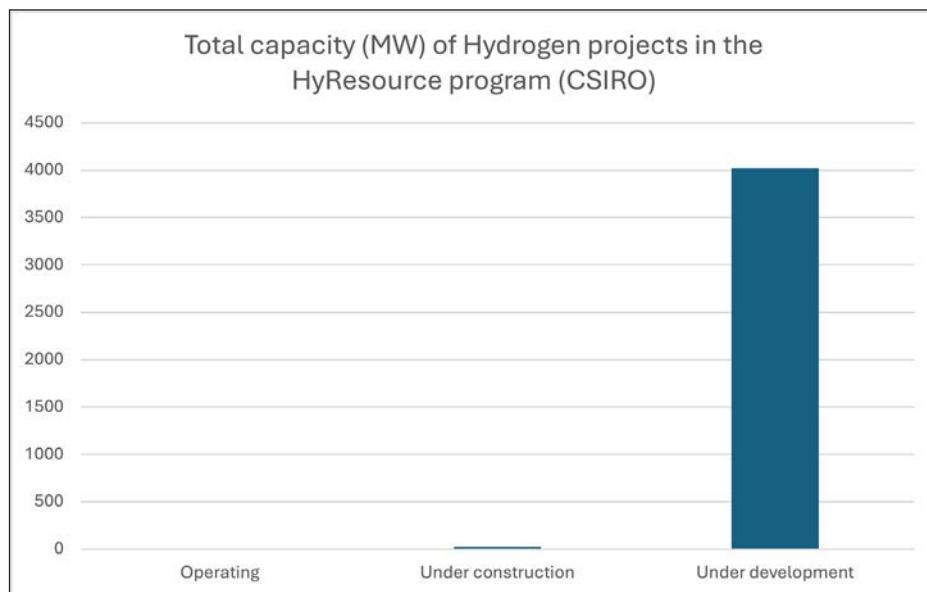
In Australia, there have been several high-profile cancellations of major projects in recent years:

Project	Location	Proponent	Date cancelled	Size & Cost
Whyalla Hydrogen Facility ³⁵	Whyalla, SA	SA government	5/5/25	250 MW, \$593 million
Nyrstar ³⁶	Port Pirie, SA	Trafigura	25/3/25	440 MW, \$750 million
Central Queensland Hydrogen Project CQH2 ³⁷	Gladstone, QLD	QLD government	30/6/25	2 GW, \$14 billion
Crystal Brook Energy Park ³⁸	Port Pirie, SA	Neoen	2024	50 MW
H2Tas ³⁹	Bell Bay, TAS	Woodside	2/9/24	300 MW
Hydrogen Energy Supply Chain (HESC) Project ⁴⁰	Latrobe Valley, VIC	Kawasaki Heavy Industries	31/3/25	\$500 million
Torrens Island Green Hydrogen Hub ⁴¹	SA	AGL	15/10/24	250 MW
HyEnergy ⁴²	Carnarvon, WA	Province Energy	4/9/24	8 GW, \$25 billion
ATCO ⁴³	Warradarge, WA	ATCO	17/8/23	10 MW
Australian Renewable Energy Hub ⁴⁴	Pilbara WA	bp	24/7/25	14 GW, \$54 billion

Despite this, there remain 87 projects still forging ahead, according to the CSIRO HyResource database.⁴⁵ Yet of these,

almost all of them are listed as 'under development' (Figure 4).

Figure 4 - Status of hydrogen projects in the CSIRO HyResource database, by capacity



Why is this? If the opportunities in Australia for hydrogen are so great, why is the

industry struggling to make headway?

3. Green hydrogen is fundamentally and immutably expensive

Green hydrogen's most basic use-case is to replace the grey or blue hydrogen in chemical manufacturing processes. The more advanced use-cases include powering fuel cells for long-haul transportation, or turning hydrogen into ammonia to power ships, but these involve extra steps of storage and transportation.

If the economics do not stack up for the most basic use case, more advanced use cases are clearly not viable, rendering optimism about future use void.

We analyse the cost for the basic use case below.

3.1 Manufacturing hydrogen is expensive

Green hydrogen's fundamental flaw is the energy intensiveness of the production process. Water is a tightly bonded molecule, and it takes a lot of energy to split the bond between hydrogen (H_2) and

oxygen (O). Chemistry sets the floor — the absolute minimum amount of energy required — of 39.4 kWh/kg H₂ at 100% efficiency,⁴⁶ with typical electrolyzers requiring around 53 kWh/kg H₂.⁴⁷ To put this into perspective, 53 kWh could lift a 1-tonne object 19.5km vertically, or power a modern electric vehicle for 350km, or power a typical home for 3 days, or run a 2kW space heater for 26 hours.

But energy is not the only expensive aspect. Electrolyzers are costly pieces of equipment, with prices ranging from \$1200-2400/kW installed capacity. There are two main types of electrolyzers — alkaline and proton exchange membrane (PEM). Alkaline is suited to steady-state operations, whereas PEM has a wider range of operation, making it more suited to fluctuating renewable power.

CSIRO's GenCost report places the cost of alkaline electrolyzers at \$2,571/kW, and PEM at \$2,734/kW.⁴⁸

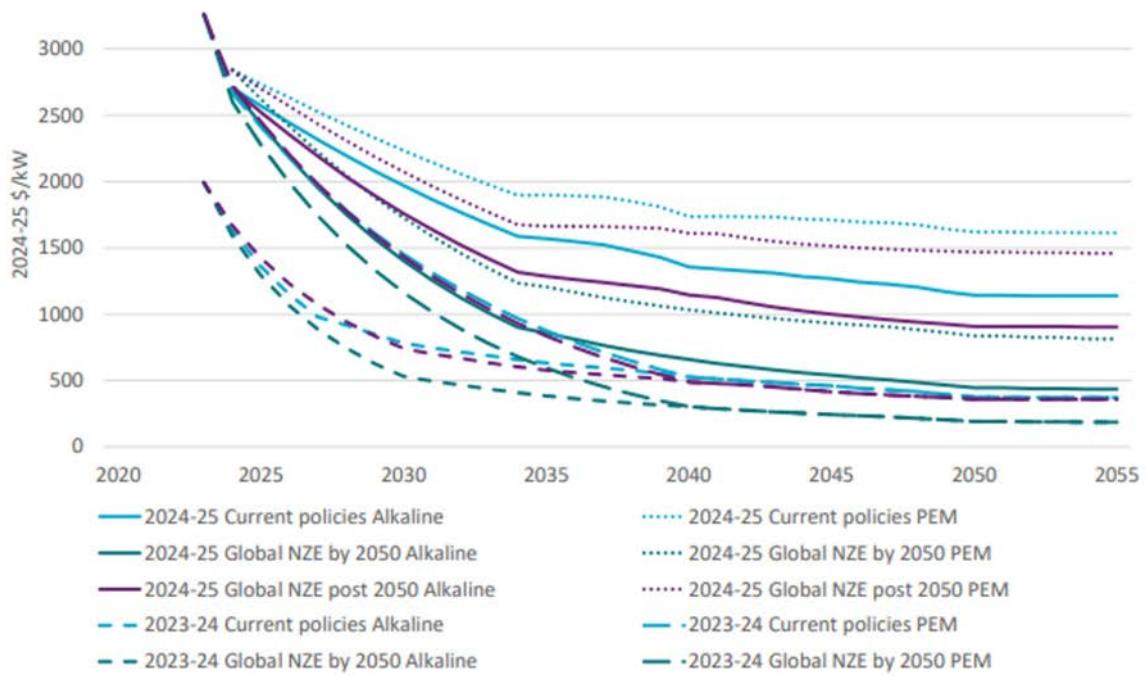
Scenario	Alkaline (\$/kW)	PEM (\$/kW)
2025	2,571	2,734
2050 current policies	1,138	1,613
2050 optimistic	435	815

Bloom Energy, an electrolyser manufacturer, gives a more optimistic cost range⁴⁹:

Scenario	Alkaline (\$/kW)	PEM (\$/kW)
2025 lower estimate	793	1,060
2025 upper estimate	1,587	2,444

The GenCost report has an optimistic cost curve for predicted future prices of hydrogen electrolyzers (Figure 5).⁵⁰

Figure 5 - CSIRO GenCost - Projected technology capital costs for alkaline and PEM electrolyzers by scenario, compared to 2023-24



We will demonstrate that even at very optimistic electrolyser prices, green hydrogen remains prohibitively expensive to produce.

3.2 Cost of steady-state green hydrogen from firmed power

Consider a simple grid-connected electrolyser. If grid (firmed) electricity is used, the electrolyser can be highly utilised

in a relatively steady state, which allows for a smaller sizing of a cheaper type of electrolyser (alkaline). However, higher power prices must be factored into this calculation to account for highly available power.

The below set of parameters were used to calculate the sensitivity of hydrogen prices to two variables: electrolyser and power prices, as shown. Appendix 1 sets out the calculations in detail.

Parameters/Inputs		
General	Discount rate	7%
	Hydrogen production energy cost	53 kWh/kg
Electrolyser	Capacity Factor	80%
	Lifetime hours	80,000 hours
	Lifetime years	11.42 years
	O&M % of capex	3%

Hydrogen levelised cost sensitivity (\$/kg)					
		Electrolyser capital cost (\$/kW)			
		2,571	1,138	435	0
Power prices (\$/kWh)	0.30	19.01	17.28	16.43	15.90
	0.23	15.20	13.46	12.61	12.08
	0.20	13.71	11.98	11.13	10.60
	0.15	11.06	9.33	8.48	7.95
	0.10	8.41	6.68	5.83	5.30
	0.05	5.76	4.03	3.18	2.65

Note that even if the electrolyser is cost-free and power prices are unrealistically low, green hydrogen is still more expensive than hydrogen from natural gas at \$2/kg.

3.3 Cost of green hydrogen from fluctuating renewable power

Alternatively, hydrogen production can play a 'solar sponge' role, absorbing

excess renewable energy when available, as planned in the ISP.⁵¹ Given solar's intermittent nature, utilisation rates are expected to drop significantly, to around 25%, in line with solar's capacity factor. A larger, more expensive electrolyser, sized according to peak generation, must also be used. Appendix 1 contains a full breakdown of the methodology for these calculations.

Parameters/Inputs		
General	Discount rate	7%
	Hydrogen production energy cost	53 kWh/kg
Solar	Amortisation lifetime	15 years
	Capacity factor	25%
Electrolyser	Capacity Factor	25%
	Lifetime hours	40000 hours
	Lifetime years	18.26 years
	O&M % of capex	3%

Again, a sensitivity analysis can be conducted:

Hydrogen levelised cost sensitivity (\$/kg)						
	Electrolyser capital cost (\$/kW)					
	2,734	2,000	1,613	815	0	
Solar capital cost (\$/kW)	1,500	12.50	10.21	9.01	6.52	3.99
	1,200	11.70	9.42	8.21	5.73	3.19
	1,000	11.17	8.89	7.68	5.20	2.66

3.4 Cost of green hydrogen from an optimised off-grid project

A more complex analysis can be undertaken to model an off-grid project using a mixture of wind and solar generation, with an under-sized electrolyser. The reason for under-sizing the electrolyser is so it can operate at utilisation rates higher than the capacity factor of the generation, although this means that some energy is wasted when the system is at peak generation. This creates a trade-off between the value of the energy wasted, and the capital cost saved on a smaller electrolyser.

The economics are also heavily affected by the correlation/anti-correlation of the wind and solar generation, and their respective

proportions in the generation mix.

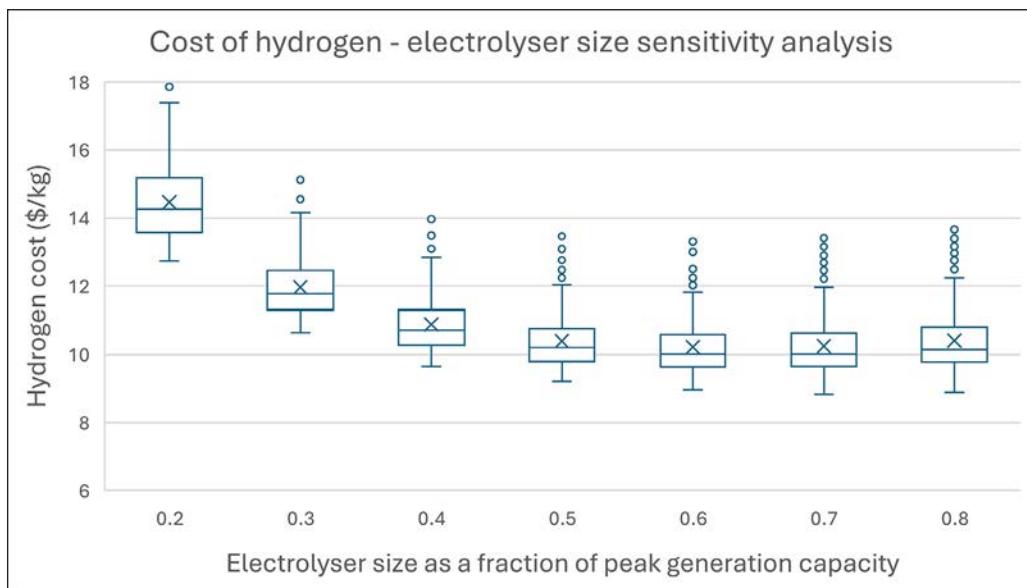
We conducted an empirical analysis with data from individual wind and solar farms. Each combination of generators was combined into a hypothetical wind and solar project, with an iteration over the proportion of each generation type in the mixture and a further iteration over electrolyser size as a proportion of peak generation.

For each of these combinations, the overall cost of hydrogen from each of these hypothetical projects was calculated. This sensitivity analysis produced 38,025 results, showing that electrolyser sizes in the range of 60% to 70% of peak generation capacity produce the cheapest hydrogen.

Parameters/Inputs for base case		
General	Discount rate	7%
	Hydrogen production energy cost	53 kWh/kg
	Amortisation lifetime	15 years
Generation	Solar cost	1500 \$/kW
	Wind cost	3200 \$/kW
	Cost	2000 \$/kW
Electrolyser	Lifetime hours	40000 hours
	O&M % of capex	1%

As above, Appendix 1 contains more details on the methodology for these calculations.

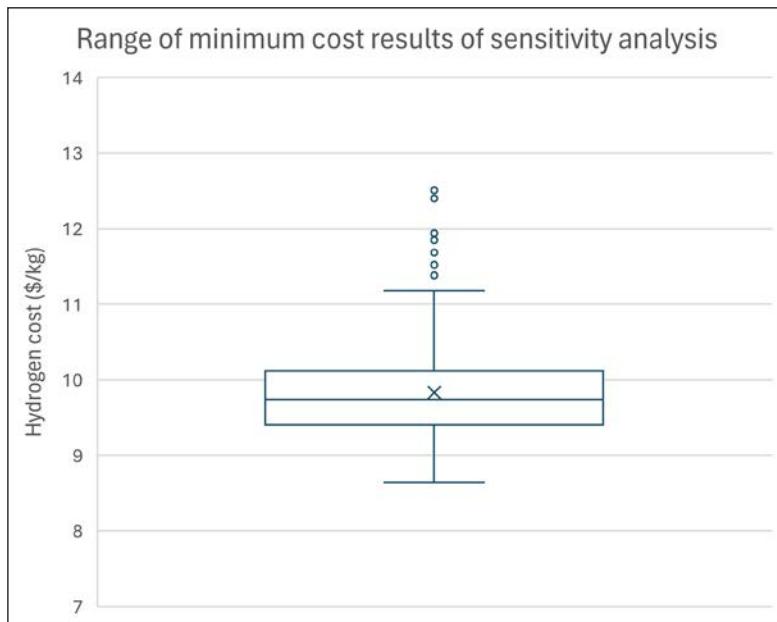
Figure 6 - Box-and-whisker plot of hydrogen costs across the sensitivity analysis



Taking only the minimum-cost scenarios for each of the combinations of wind and

solar farms, we can construct the range of minimum-cost outcomes:

Figure 7 - Box-and-whisker plot of minimum-cost hydrogen across the sensitivity analysis

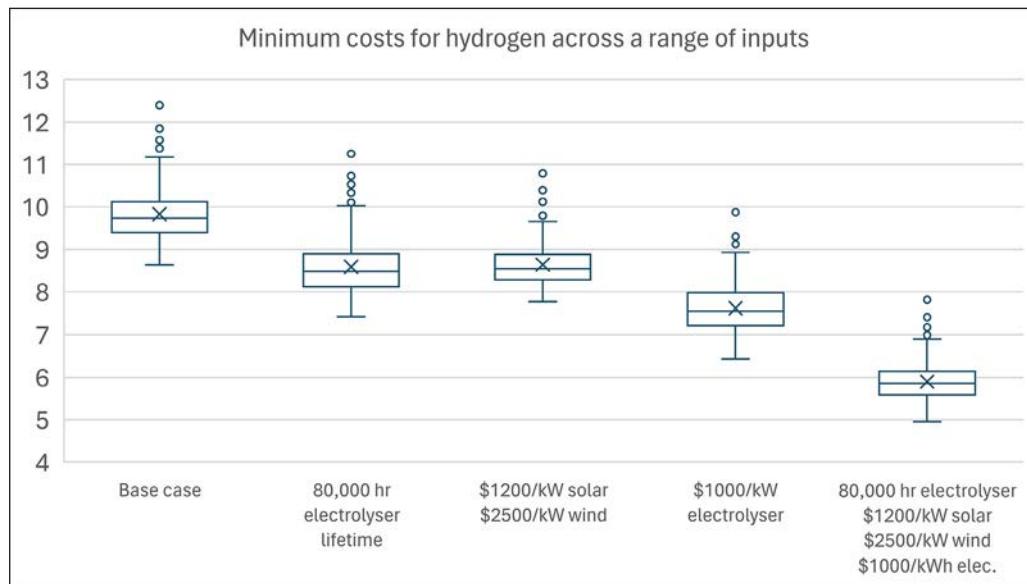


It is not realistic to assume that this minimum can be designed for, since this would require perfect foresight of weather patterns many years in advance.

We conclude that off-grid optimised hydrogen cost is in the range of \$10/kg.

For completeness' sake, we also calculate results for a range of changes to the input variables. The most optimistic set of input variables yields a cost estimate in the range of \$6/kg.

Figure 8 - Box-and-whisker plots for cost of hydrogen across sensitivities of input variables



3.5 Scale will not solve these problems

From the above analyses, even extremely optimistic future scenarios fail to render green hydrogen cost competitive with natural gas.

In most realistic cases, the price for green hydrogen is over \$10/kg — 500% of the current market price of grey hydrogen. This means that for projects to be successful, they must either find a buyer at \$10/kg or receive subsidies of \$8/kg.

Economies of scale and technological developments can only go so far to ameliorate green hydrogen's basic cost, which is driven by physics. Arguments to the contrary must necessarily be propped up by wishful thinking.

3.6 More advanced uses simply add more cost

The above analysis considers green hydrogen for industrial chemical use only — manufactured and used on-site, integrated into existing production. This does not

include the storage, transportation and end-use costs and inefficiencies associated with more advanced uses for green hydrogen.

Touted as a panacea for hard-to-electrify applications like long-haul freight, shipping, and steelmaking, hydrogen underpins the final stage of net-zero ambitions.

One of the key challenges for these applications is storage. Hydrogen is the lightest element, and hard to compress. At atmospheric pressure and standard temperature, it has a density of 0.083 kg/m³ — just 7% the density of air, and 0.0097% the density of diesel.

Compressing hydrogen to 70 MPa can raise the density to 40 kg/m³, but this alone costs 12% of its energy content.⁵² Liquefying hydrogen is even more difficult, costing 36% of the energy content, and requiring extremely low temperatures of -252°C.⁵³

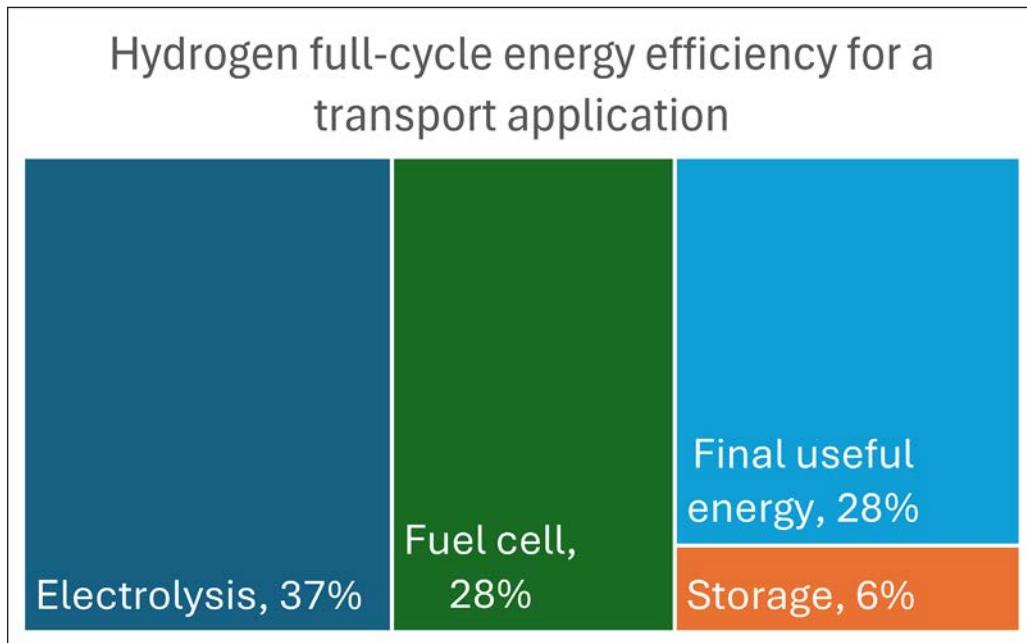
The low density is only partially offset by the high energy content — 1 kg of hydrogen has more than 2.6 times the energy of 1kg of diesel. The energy in 200L

of diesel could be replaced by 900L of liquid hydrogen, or 1600L of pressurised gaseous hydrogen at 70MPa.

For transport, the final use of this hydrogen

is in a fuel cell, which produces electricity to power a motor. The round-trip efficiency of hydrogen for this application is less than 30%, with Figure 6 demonstrating the components of the losses.⁵⁴

Figure 9 - Hydrogen round trip energy efficiency for transport applications



Other impediments to widespread use include:

- Highly flammable and deflagration-prone, with very little ignition energy required. It also has a wide flammability range — flammable in air from about 4% to 75% concentration, which is much wider than most fuels (methane, for example is flammable from 5% to 15%). All these factors make it difficult to store and use safely;
- Embrittlement — causes metals to become more brittle, leading to more cracking and fracturing. Tanks and pipes must be inspected and replaced more often, leading to higher costs.

electrolyzers, as well as more efficient fuel cells and distribution routes for hydrogen fuel, etc. For this reason, we have included even what we consider to be unrealistically optimistic inputs in our sensitivity analysis. Indeed, many of these improvements may be eventually achieved, but our analysis indicates that hydrogen would remain relatively expensive.

The overarching point of this paper is that to pin a nation's future on the expectations of improvements in an emerging technology is fundamentally foolish. It would make more sense to wait until these improvements materialise, and to then incorporate them into our plans.

3.7 Addressing more optimistic cost assumptions

Although we have cited what we believe to be reasonable figures for the input costs and assumptions in the above calculations, some critics may state that technological development and economies of scale will bring lower cost and higher efficiency

4. The Orica deal exposes the plan as untenable

As Australia's largest chemical manufacturer, Orica uses hydrogen extensively to produce explosives for the mining industry, as well as fertilisers for agriculture.

The federal government recently announced \$432 million of funding for Orica's Hunter Valley Hydrogen project.¹⁵ The funding is for a 50 MW electrolyser which will produce roughly 4,700 tonnes of green hydrogen annually. This represents 7.5% of Orica's existing hydrogen use. This grant is in addition to prior announcements of \$45 million of state¹⁶ and \$70 million of federal funding,¹⁷ bringing the total subsidy for this project to \$547 million.

Orica CEO Sanjeev Ghandi acknowledged that green hydrogen cannot currently be made economically and requires subsidies for both capital and operational expenditure. However, he justified accepting government subsidies by suggesting scale and experience will bring costs down and make the process more economically competitive over time.⁵⁵ It is doubtful whether the future holds radically cheaper production costs. As we have already shown, much of the cost structure of green hydrogen is determined by factors extrinsic to scale and experience, such as energy prices. The Orica application is the most basic green hydrogen use case — it should be cheapest and easiest to achieve integration into chemical production first. Instead, the converse is proving true: that if green hydrogen doesn't make sense in this use-case, there is little hope for every other use case.

4.1 Implicit subsidised hydrogen price

The subsidy of \$547m equates to an annual value of \$52m over 20 years at a 7% discount rate. The plant will produce 4,700 tonnes of green hydrogen annually, which means that each kilogram of green hydrogen is worth \$10.99 in subsidies. This is well over the stated \$2/kg 'Hydrogen Production Tax Incentive' subsidy which is current government policy.⁵⁶

Scaling up the implied subsidies, it would take an equivalent subsidy of \$7.3b to justify Orica replacing all of its hydrogen

requirements with green hydrogen. Replacing Australia's current industrial hydrogen usage of 500,000 tonnes per annum would require \$58b. Achieving the capacity required for Green Energy Exports of 15 million tonnes of hydrogen production annually would require \$3.19t.

4.2 Implicit price of carbon abatement

So-called 'grey' hydrogen is made from natural gas, without carbon capture. The base chemical ratios of the process dictate that at least 5.5 kg of H₂ is produced for every kg of CO₂. Including inefficiencies and process heat, the number is closer to 7 kg CO₂/kg H₂.⁵⁷ Including other lifecycle factors all the way from the source such as drilling, methane leakage, storage, and transport, an estimated 12kg of CO₂ equivalents are released for every kg of hydrogen.⁵⁸

With this data, we can calculate the number of tonnes of CO₂ abated using the Orica subsidy. We know that the plant will produce 4,700 tonnes of green hydrogen annually, which amounts to between 32,900 and 56,400 tonnes of CO₂ abated. The annual value of the subsidy over 20 years, at a 7% discount rate is \$52m.

Therefore, the cost of abatement is at the lowest \$915/tonne CO₂, and at the highest \$1,569/tonne CO₂. To put this in context, Australian Carbon Credit Unit (ACCU) prices have been averaging between \$30-\$40/tonne CO₂ for the last few years.⁵⁹ This means the Orica subsidy represents carbon abatement at a cost 26 to 44 times higher than existing projects. In no way can this subsidy — or for that matter, any hydrogen subsidies — be construed as being in the public interest.

Conclusion

Green hydrogen's role as a linchpin in Australia's net zero strategy is untenable. There is no remaining rationale for the continued planning and funding of green hydrogen projects. The \$477m subsidy for Orica's Kooragang Island project reveals the stark economic realities of green hydrogen production. At \$9.57/kg in subsidies, the cost far exceeds the market price of grey hydrogen (\$2/kg), with abatement costs of \$798-\$1,368/tonne CO₂, dwarfing typical carbon credit prices. These figures highlight that green hydrogen, even in its simplest application, requires massive financial support to be viable.

The energy-intensive nature of electrolysis, high capital costs, and inefficiencies in storage and transport — driven by hydrogen's low density and material challenges — render it uncompetitive without sustained subsidies.

The failure of numerous high-profile projects and the stalled progress of most others in Australia's hydrogen pipeline further underscore these challenges.

Scaling green hydrogen to meet national or export goals would demand trillions in subsidies. Proponents of green hydrogen might argue that the subsidies would never amount to trillions because they will kick-start innovation and investment that will eventually make hydrogen so cheap that subsidies are no longer required. In contrast, we have shown that the cost challenges are fundamental and largely extrinsic to scale.

The Orica deal is a cautionary tale: rather than a stepping stone to a green superpower, it exposes green hydrogen as a costly and inefficient solution, propped up by wishful thinking rather than economic or physical reality.

Yet it remains the government's official plan to give hydrogen a critical role in the energy system of the future. Policymakers must reassess hydrogen's role in the energy transition and prioritise more viable decarbonisation pathways.

The only thing worse than beating a dead horse is betting on one. When the wager is Australia's future, hydrogen is simply a bad bet.

Appendix 1 — Detailed hydrogen costing analysis

First, we must distinguish between firmed and unfirmed power. Firmed power allows an operator to utilise their assets at a high rate (we use 80%), so they can purchase a smaller, cheaper electrolyser suited to steady-state operation. They must, however, pay the going rate for firmed electricity.

Using unfirmed power is more in line with the intentions for hydrogen in the ISP, which utilises hydrogen electrolyzers as load sinks in the system, opportunistically soaking up the excess renewable electricity. This implies a very low utilisation rate, as the electrolyser will only be used when there is ample renewable generation *and* the power is not required by the grid (typically during peak solar hours). The multiplication of these two rates could be a low number indeed. However, for simplicity, we will model a solar-only standalone

project, which installs renewable electricity with the intention to use 100% of the power generated, whenever it is generated, to make hydrogen. This means the utilisation rate will be the same as the capacity factor for the renewable generation, and the electrolyser must be sized to the maximum generation capacity of the renewable energy source.

The final stage of analysis is modelling a more complex off-grid project, similar to Murchison,⁶⁰ in WA. This type of project typically uses a mixture of wind and solar, and under-sizes the electrolyser so that it achieves a higher utilisation rate, although this means that energy is wasted when the system is at peak generation.

Below are worked examples using the numbers from the announced Orica subsidy.

Throughout, we make use of the present-value/annuity formula to annualise up-front costs. Briefly, it is:

$$PV = \sum \frac{\text{annual amount}}{(1 + r_{\text{discount}})^n}$$

This can be solved for the annual amount, given a time period and a discount rate.

A1.1 Firmed grid electricity

Electrolyser sizing

Assumptions/inputs:

1. Utilisation rate is 80%
2. Energy cost of electrolysing hydrogen is 53 kWh/kg

We can solve for the required size of electrolyser by choosing an annual output of 4,700 tonnes.

annual output=hours in year·utilisation rate·hourly hydrogen output

$$H_{\text{annual}} = h_{\text{year}} \cdot u \cdot H_{\text{hourly}}$$

Where:

H_{annual} is the annual hydrogen output (kg)

h_{year} is the number of hours in a year

u is the utilisation rate of the electrolyser

H_{hourly} is the hourly output of hydrogen (kg), determined by electrolyser size and efficiency, assuming full power is supplied:

$$H_{hourly} = \frac{L_{size}}{E_{in}}$$

Where:

L_{size} is the size of the electrolyser (kW)

E_{in} is the energy input required to make 1 kg of hydrogen. (kWh/kg)

So,

$$H_{annual} = \frac{h_{year} \cdot u \cdot L_{size}}{E_{in}}$$

For the Orica project:

$$L_{size} = \frac{4700000 \text{ kg}}{365 \cdot 24 \cdot 0.8} \cdot 53 \text{ kWh/kg}$$

$$L_{size} = 35,545.09 \text{ kW} \approx 35.5 \text{ MW}$$

Electrolyser cost

Assumptions/inputs:

1. Alkaline electrolyser used - suited for baseload operations
2. Electrolyser capital cost \$1200/kW
3. Electrolyser lifetime 80,000 hours (11.42 years at 80% utilisation)
4. Discount rate 7%
5. Operation and maintenance costs 3% of capital costs annually

The capital cost component is simply the size of the electrolyser multiplied by its per-kW cost.

$$C_{capex} = L_{size} \cdot C_{per_kW}$$

$$C_{capex} = 35,500 \cdot 1200 = \$42.6m$$

An annual repayment/equivalent value can be calculated using the same annuity method as above, which is a function of the lifetime, capital cost, and discount rate.

$$C_{capex_annual} = f(C_{capex}, t_{lifetime}, r)$$

This can be expressed as a percentage of the overall capex.

$$x_{annual_percent} = \frac{C_{capex_annual}}{C_{capex}}$$

Or,

$$C_{capex_annual} = C_{capex} \cdot x_{annual_percent}$$

We can also incorporate an annual operation and maintenance cost, expressed as a percentage of the overall capex.

$$C_{O\&M_annual} = x_{O\&M_percent} \cdot C_{capex}$$

For our example,
 $C_{capex_annual} = \$3,731,760$

$$C_{O\&M_annual} = 3\% \cdot \$42.6m = \$1,278,000$$

This gives total electrolyser annual costs of:

$$C_{total_annual} = \$5,009,760$$

If we divide this by annual output, we can already arrive at a per-kg cost for electrolyser equipment:

$$C_{per_kg} = \frac{C_{total_annual}}{H_{annual}} = \frac{C_{capex} \cdot (x_{annual_percent} + x_{O\&M_percent})}{H_{annual}}$$

$$C_{per_kg} = \frac{L_{size} \cdot C_{per_{kW}} \cdot (x_{annual_percent} + x_{O\&M_percent})}{H_{annual}}$$

For our example

$$C_{per_kg} = \frac{C_{total_annual}}{H_{annual}} = \frac{\$5,009,760}{4,700,00} = \$1.07/kg$$

Energy Cost

Assumptions/inputs

1. Firmed electricity cost \$0.23/kWh

Total energy used in a year, J_{annual} (kWh), can be calculated:

$$J_{annual} = L_{size} \cdot u \cdot h_{year}$$

For our example, at 80% utilisation:

$$J_{annual} = 35,500 \text{ kW} \cdot 0.8 \cdot 365 \cdot 24 \text{ h} = 248784000 \text{ kWh}$$

At a power price, p_{power} , of \$0.23/kWh, this gives an annual energy cost:

$$E_{annual} = J_{annual} \cdot p_{power} = 248784000 \text{ kWh} \cdot 0.23 \text{ \$/kW}$$

$$E_{annual} = \$56,722,752$$

Again, this can be translated into a per-kg cost:

$$E_{per_kg} = \frac{E_{annual}}{H_{annual}}$$

$$E_{per_kg} = \frac{\$56,722,752}{4,700,00} = \$12.08/kg$$

Total cost

The total cost per kilogram of hydrogen produced is simply the sum of the capital and energy cost components.

$$\text{Total hydrogen cost per kg} = HC_{per_kg} = C_{per_kg} + E_{per_kg}$$

$$HC_{per_kg} = 1.07 + 12.08 = \$13.15/kg$$

Leaving all input variables in, we can express the total cost as:

$$HC_{per_kg} = \frac{C_{total_annual}}{H_{annual}} + \frac{E_{annual}}{H_{annual}}$$

$$HC_{per_kg} = \frac{C_{capex_annual} + C_{O\&M_annual}}{H_{annual}} + \frac{J_{annual} \cdot p_{power}}{H_{annual}}$$

$$HC_{per_kg} = \frac{L_{size} \cdot C_{per_kW} \cdot (x_{annual_percent} + x_{O\&M_percent})}{H_{annual}} + \frac{L_{size} \cdot u \cdot h_{year} \cdot p_{power}}{H_{annual}}$$

$$HC_{per_kg} = \frac{L_{size} [C_{per_kW} \cdot (x_{annual_percent} + x_{O\&M_percent}) + u \cdot h_{year} \cdot p_{power}]}{H_{annual}}$$

Remembering:

$$H_{annual} = \frac{h_{year} \cdot u \cdot L_{size}}{E_{in}}$$

Substituting:

$$HC_{per_kg} = \frac{E_{in} [C_{per_kW} \cdot (x_{annual_percent} + x_{O\&M_percent}) + u \cdot h_{year} \cdot p_{power}]}{h_{year} \cdot u}$$

And recalling our variable definitions:

h_{year} is the number of hours in a year

u is the utilisation rate of the electrolyser

E_{in} is the energy input required to make 1 kg of hydrogen (kWh/kg).

C_{per_kg} is the electrolyser capital cost

$x_{annual_percent}$ is the annual amortisation of the capex, expressed as a percentage of the total capex

$x_{O\&M_percent}$ is the annual operation and maintenance cost, expressed as a percentage of the total capex

p_{power} is the electricity price (\$/kWh)

A1.2 Unfirmed renewables — simple

Energy generation sizing

Assumptions/inputs:

1. *Choice of renewable energy: Solar or wind or some combination.*
For simplicity, we choose solar only.
2. *Capacity factor of generation. We use 25%.*

We are able to size the required generation by working backwards from the output. We start by calculating the total annual energy required to make our desired annual output of 4,700 tonnes of hydrogen.

$$J_{annual} = H_{annual} \cdot E_{in}$$

$$J_{annual} = 4,700,000 \text{ kg} \cdot 53 \text{ kWh/kg} = 249,100,000 \text{ kWh}$$

We can then work backwards using the capacity factor to arrive at the sizing of the system.

$$J_{annual} = c \cdot S_{size} \cdot h_{year}$$

Where,

c is the solar capacity factor.

S_{size} is the solar system size (kW)

h_{year} is the hour in year.

$$S_{size} = \frac{J_{annual}}{c \cdot h_{year}}$$

$$S_{size} = \frac{249,100,000 \text{ kWh}}{0.25 \cdot 365 \cdot 24} = 113,744 \text{ kW}$$

Energy generation cost

Assumptions/inputs:

1. *Cost of generation: We use GenCost \$1500/kW.*
2. *Lifetime of asset: We use 15 years.*
3. *Discount rate: We use 7%.*

$$S_{cost} = S_{size} \cdot C_{solar_perkW}$$

Where,

S_{cost} is the cost of the solar system.

C_{solar_perkW} is the cost per kW of solar generation.

Using the GenCost numbers of \$1500/kW, a 113 MW system would cost.

$$S_{cost} = S_{size} \cdot C_{solar_per kW}$$

$$S_{cost} = 113,744 \text{ kW} \cdot 1,500 \text{ \$/kW}$$

$$S_{cost} = \$170,616,573$$

Using the same annuity method we've used throughout, this equates to an annual equivalent of:

$$S_{cost_annual} = f(S_{cost}, t_{lifetime}, r)$$

This can be expressed as a percentage of the overall capex.

$$x_{solar_annual_percent} = \frac{S_{cost_annual}}{S_{cost}}$$

Or,

$$S_{cost_annual} = S_{cost} \cdot x_{solar_annual_percent}$$

So our annual solar system cost is:

$$S_{cost_annual} = \$18,732,783$$

Note that this produces an implied cost of energy of:

$$\text{implied cost of energy} = \frac{\text{annual cost}}{\text{annual energy}} = \frac{\$18,732,783}{249,100,000 \text{ kWh}} = \$0.075/\text{kWh}$$

We can also arrive at a per-kg energy cost of hydrogen.

$$E_{per_kg} = \frac{S_{cost_annual}}{H_{annual}} = \frac{\$18,732,783}{4,700,000} = \$3.99/\text{kg}$$

Generalising,

$$E_{per_kg} = \frac{S_{cost} \cdot x_{solar_annual_percent}}{H_{annual}}$$

$$E_{per_kg} = \frac{S_{size} \cdot C_{solar_per kW} \cdot x_{solar_annual_percent}}{H_{annual}}$$

$$E_{per_kg} = \frac{\frac{J_{annual}}{c \cdot h_{year}} \cdot C_{solar_per kW} \cdot x_{solar_annual_percent}}{H_{annual}}$$

$$E_{per_kg} = \frac{\frac{H_{annual} \cdot E_{in}}{c \cdot h_{year}} \cdot C_{solar_per kW} \cdot x_{solar_annual_percent}}{H_{annual}}$$

$$E_{per_kg} = \frac{E_{in} \cdot C_{solar_per kW} \cdot x_{solar_annual_percent}}{c \cdot h_{year}}$$

Electrolyser sizing

Electrolyser must be sized according to the maximum power output of generation. If the electrolyser is any smaller, then we cannot fully utilise the power at peak times. An alternative arrangement would be to use firming to absorb this power and then use it at non-peak times, which would of course introduce firming costs. We do not model this scenario here.

We can solve for the required size of electrolyser by choosing an annual output of 4700 tonnes.

$$L_{size} = S_{size} = 113,744 \text{ kW}$$

Electrolyser cost

Assumptions/inputs:

1. *Electrolyser type required is Proton Exchange Membrane (PEM) due to the need for fast reaction time to variable generation.⁶¹*
2. *Electrolyser capital cost \$2000/kW*
3. *Electrolyser lifetime 40,000 hours⁶² (18.26 years at 25% utilisation)*
4. *Discount rate 7%*
5. *Operation and maintenance costs 3% of capital costs annually*

The capital cost component is simply the size of the electrolyser multiplied by its per-kW cost.

$$C_{capex} = L_{size} \cdot C_{per_kW}$$

$$C_{capex} = 113,744 \cdot 2000 = \$227,000,000$$

An annual repayment/equivalent value can be calculated using the same annuity method as above, which is a function of the lifetime, capital cost, and discount rate.

$$C_{capex_annual} = f(C_{capex}, t_{lifetime}, r)$$

This can be expressed as a percentage of the overall capex.

$$x_{annual_percent} = \frac{C_{capex_annual}}{C_{capex}}$$

Or,

$$C_{capex_annual} = C_{capex} \cdot x_{annual_percent}$$

$$C_{capex_annual} = \$22,447,744$$

We can also incorporate an annual operation and maintenance cost, expressed as a percentage of the overall capex.

$$C_{O\&M_annual} = x_{O\&M_percent} \cdot C_{capex}$$

For our example,

$$C_{O\&M_annual} = 3\% \cdot \$227m = \$6,824,663$$

So to arrive at the total,

$$C_{total_annual} = C_{capex_annual} + C_{O\&M_annual}$$

$$C_{total_annual} = C_{capex} \cdot (x_{annual_percent} + x_{O\&M_percent}) = \$29,272,407$$

If we divide this by annual output, we can already arrive at a per-kg cost for electrolyser equipment:

$$C_{per_kg} = \frac{C_{total_annual}}{H_{annual}} = \frac{C_{capex} \cdot (x_{annual_percent} + x_{O\&M_percent})}{H_{annual}}$$

$$C_{per_kg} = \frac{L_{size} \cdot C_{per_kW} \cdot (x_{annual_percent} + x_{O\&M_percent})}{H_{annual}}$$

For our example:

$$C_{per_kg} = \frac{C_{total_annual}}{H_{annual}} = \frac{\$29,272,407}{4,700,00} = \$6.23/kg$$

Total cost

The total cost per kilogram of hydrogen produced is simply the sum of the capital and energy cost components.

$$Total\ hydrogen\ cost\ per\ kg = HC_{per_kg} = C_{per_kg} + E_{per_kg}$$

$$HC_{per_kg} = 6.23 + 3.99 = \$10.21/kg$$

Leaving all input variables in, we can express the total cost as:

But recall,

$$C_{per_kg} = \frac{L_{size} \cdot C_{per_kW} \cdot (x_{annual_percent} + x_{O\&M_percent})}{H_{annual}}$$

And,

$$E_{per_kg} = \frac{E_{in} \cdot C_{solar\ per\ kW} \cdot x_{solar\ annual\ percent}}{c \cdot h_{year}}$$

So,

$$HC_{per_kg} = \frac{L_{size} \cdot C_{per_kW} \cdot (x_{annual_percent} + x_{O\&M_percent})}{H_{annual}} + \frac{E_{in} \cdot C_{solar\ per\ kW} \cdot x_{solar\ annual\ percent}}{c \cdot h_{year}}$$

Remembering:

$$L_{size} = S_{size} = \frac{J_{annual}}{c \cdot h_{year}} = \frac{H_{annual} \cdot E_{in}}{c \cdot h_{year}}$$

Therefore:

$$HC_{per_kg} = \frac{E_{in} \cdot C_{electrolyser\ per\ kW} \cdot (x_{electrolyser\ annual\ percent} + x_{O\&M_percent})}{c \cdot h_{year}} + \frac{E_{in} \cdot C_{solar\ per\ kW} \cdot x_{solar\ annual\ percent}}{c \cdot h_{year}}$$

$$HC_{per_kg} = \frac{E_{in}}{c \cdot h_{year}} [C_{electrolyser\ per\ kW} \cdot (x_{electrolyser\ annual\ percent} + x_{O\&M_percent}) + C_{solar\ per\ kW} \cdot x_{solar\ annual\ percent}]$$

And recalling our variable definitions:

h_{year} is the number of hours in a year

c is the capacity factor of solar generation, which also equals the utilisation rate of the electrolyser

E_{in} is the energy input required to make 1 kg of hydrogen (kWh/kg).

c is the electrolyser capital cost (\$/kW capacity)

$C_{electrolyser\ per\ kW}$ is the annual amortisation of the electrolyser capex, expressed as a percentage of the total capex

$x_{O\&M_percent}$ is the annual electrolyser operation and maintenance cost, expressed as a percentage of the total capex

$C_{solar\ per\ kW}$ is the solar generation capital cost (\$/kW capacity)

$x_{solar\ annual\ percent}$ is the annual amortisation of the solar generation capex, expressed as a percentage of the total capex

A1.3 Unfirmed renewables — with generation mix and undersized electrolyser

A more complex analysis can be undertaken to model an off-grid project using a mixture of wind and solar generation, with an under-sized electrolyser. The reason for under-sizing the electrolyser is so that it can operate at higher utilisation rates than the capacity factor of the generation, although this means that energy is wasted when the system is at peak generation. This is a complex trade-off between the value of the energy wasted, and the capital cost saved on a smaller electrolyser.

The economics are also heavily affected by the correlation/anti-correlation of the wind and solar generation, and their respective proportions in the generation mix.

Empirical analysis of realistic utilisation rates

We conducted an empirical analysis with data from AEMO archives⁶³ for 15 wind farm Dispatchable Unit Identifiers (DUIDs)

and 15 single-axis tracking solar farm DUIDs. Each combination of generators was combined into a hypothetical wind and solar project, where the generated electricity for each timestamp over a year was a combination of the two sources.

The number of total combinations was limited to 15 of each type as this was deemed a reasonable number to estimate the range of possible combinations. It is assumed some combinations would overestimate the benefit from anti-correlation between wind and solar, and some would underestimate it.

For each combination, we iterated over varying proportions of each generation type in the mixture from 30%/70% solar/wind to 70%/30%. We then iterated over a series of electrolyser sizes, from 20% of peak generation to 80%.

For each of these combinations, the overall utilisation rate of the electrolyser was calculated. Utilisation rates increase as the size of the electrolyser decreases, so there is no optimum size to maximise utilisation. Electrolyser cost decreases with size, but so does output. Hence we must apply the cost calculations from A1.2 above to calculate the overall cost of hydrogen from each of these hypothetical projects.

Calculating cost across generation and electrolyser size scenarios

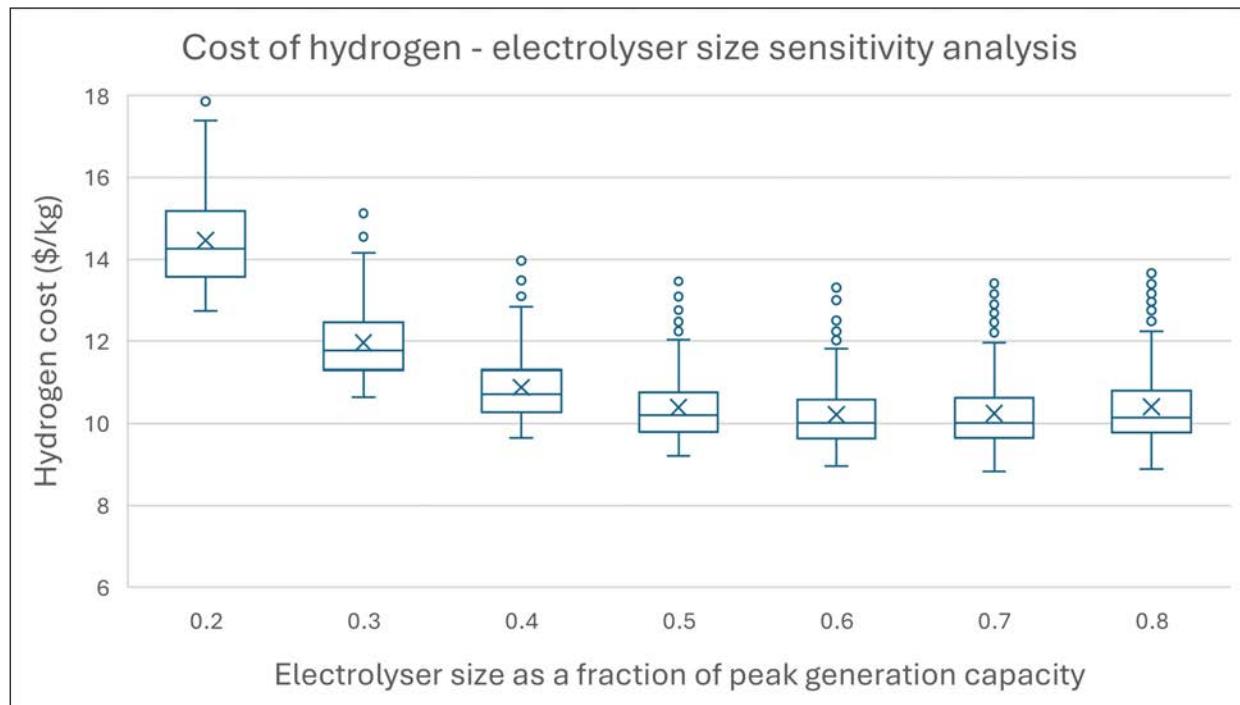
The same assumptions are used as above:

Assumptions/inputs:

1. *Cost of solar generation: We use GenCost \$1500/kW.*
2. *Cost of wind generation: We use GenCost \$3200/kW.*
3. *Lifetime of asset: We use 15 years.*
4. *Discount rate: We use 7%.*
5. *Electrolyser type required is proton exchange membrane (PEM) due to the need for fast reaction time to variable generation.⁶⁴*
6. *Electrolyser capital cost \$2000/kW*
7. *Electrolyser lifetime 40,000 hours⁶⁵*
8. *Operation and maintenance costs 1% of capital costs annually*

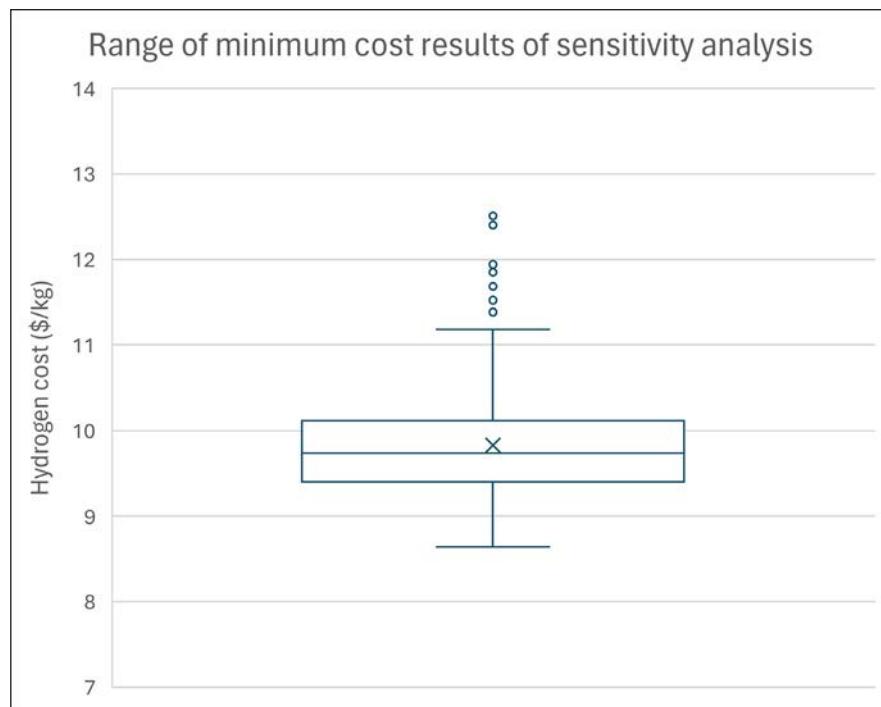
This sensitivity analysis produced 38,025 results ($15 \times 15 \times 13$ weighting parameters \times 13 load size parameters). The results show that electrolyser sizes in the range of 50% to 75% of peak generation capacity produce the cheapest hydrogen.

Figure 10 - Box-and-whisker plot of hydrogen costs across the sensitivity analysis



Taking only the minimum-cost scenarios for each of the 225 combinations of wind and solar farms, we can construct the range of minimum-cost outcomes:

Figure 11 - Box-and-whisker plot of minimum-cost hydrogen across the sensitivity analysis

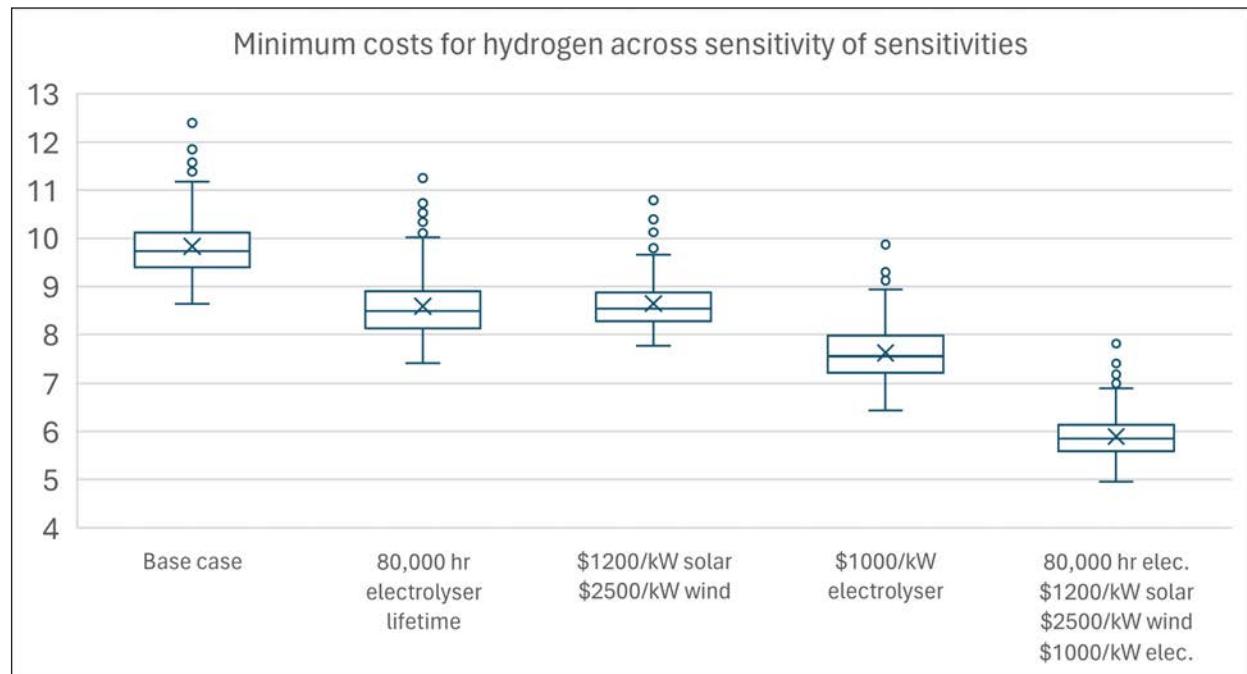


It is not realistic to assume that this minimum can be designed for, since this would require perfect foresight of weather patterns many years in advance.

We conclude that off-grid optimised hydrogen costs in the range of \$10/kg.

For the sake of completeness, we also calculate results for a range of changes to the input variables. The most optimistic set of input variables yields a cost estimate in the range of \$6/kg.

Figure 12 - Box-and-whisker plots for cost of hydrogen across sensitivities of input variables



Data and R/Python scripts for these calculations are available on request.

Summary

	Grid	Off-grid renewables - simple	Off-grid renewables - optimised
Power (\$/kWh)	\$0.23	\$0.075	-
Electrolyser type	Alkaline	PEM	PEM
Electrolyser (\$/kW)	1200	2000	2000
Energy cost component (\$/kg)	\$12.08	\$3.99	-
Electrolyser cost component (\$/kg)	\$1.07	\$6.23	-
Total Hydrogen Cost (\$/kg)	\$13.15	\$10.21	\$10

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Green hydrogen is often heralded as a cornerstone of Australia's net zero ambitions, but the reality is that it is not viable today, and won't be in the foreseeable future. This paper examines the reasons green hydrogen will likely remain prohibitively expensive, why projects are stalling, and how the recently announced Orica subsidy exposes Australia's strategy as untenable.

Hydrogen is intended to play a critical role in Australia's decarbonisation plans. Beyond replacing grey hydrogen (produced from natural gas) in chemical manufacturing, green hydrogen — produced via electrolysis using renewable energy — is envisioned for advanced applications like green metals production, long-haul transport, and electricity grid support.

However, green hydrogen's high production costs and operational challenges threaten these ambitions. The fundamental issue lies in the energy-intensive nature of electrolysis. This energy demand, coupled with high capital costs for electrolyzers, makes green hydrogen expensive. Further inefficiencies in storage and transport — driven by hydrogen's low density and material challenges — render it uncompetitive without sustained subsidies.

Yet it remains the government's official plan to give hydrogen a critical role in the energy system of the future. Policymakers must reassess hydrogen's role in the energy transition to prevent us committing today to investments and strategies which have no real prospect of success.

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